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# THERMAL ANALYSIS OF MEMS-BASED THERMOELECTRICALLY CONTROLLED MICRONOZZLE

BY

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### ABSTRACT

A new technique which implements heating upstream of the micronozzle throat and cooling downstream of the throat through the side-walls of the micronozzle is proposed. Thermoelements are used to pump heat from the cold section (supersonic) to the hot section (subsonic) of the micronozzle using Peltier effect. The proposed micronozzle is given herein the name Thermo-electrically Controlled Micronozzle (TECMN). A generalized quasi-one-dimensional model is developed to solve the flow of gaseous propellant inside the micronozzle in the presence of heat pumping from the supersonic to the subsonic through the side walls. The improvement in the efficiency due to using TECMN is verified, which is more significant for reduced divergent wall temperature and mass flow rate. The model also involves the thermoelectricity effects in the solid walls. A general energy equation of one-dimensional heat transfer in a non-uniform wall subjected to a longitudinal electrical field and lateral heat convection is developed and solved analytically for uniform wall and numerically for non-uniform walls. A set of non-dimensional parameters which affects the performance of the TECMN are identified and studied for better heat exchange with the flowing gas. It is found that the uniform TE wall performs better than non-uniform wall in heating-cooling process. The two-dimensional laminar Navier-Stokes equations are solved numerically for gas flow in a micronozzle for different thermal boundary conditions; isothermal divergent wall, uniform heating, and non-uniform heating-cooling in uniform side-walls. The non-uniform heating-cooling boundary condition is a imitation of the thermoelectric wall. It is found that heating upstream the throat always affect mass flow rate, while heating downstream the throat increases the thrust which may decrease with any mass flow reduction, however the thrust per unit mass flow and viscous losses increase always with heating. It is found that heat supply in the convergent-divergent side-wall results in enhancement of thrust level, specific impulse, mass consumption saving, and efficiency of specific impulse. Outcome of heat developing to/absorbing from a gas flowing into a convergentdivergent micronozzle for a range of Reynolds numbers below 10<sup>3</sup> is investigated assuming one-dimensional thermal analysis of a uniform side-wall. It was found that the improvement in the specific impulse efficiency increases with decreasing Reynolds number. This improvement reaches up to 9.35% at Re = 15 during the heating-cooling process through the side-walls. Heating process and heating-cooling process through the wall are more useful to improve efficiency at low Reynolds numbers below 100. This research concludes that the utilization of thermoelectricity to supply heat upstream of micronozzle throat and remove heat downstream of throat through thermoelement side walls is very useful to improve the micronozzle efficiency and reduces propellant consumption.

### خلاصة البحث

المنافث الدقيقة تعانى من خسائر لزوجة الغاز وخاصة عند ارقام Reynolds المنخفضة. بعد عمل استقصاء ودراسة انظمة الدفع الميكانيكية المستخدمة، تم اقتراح تقنية جديدة وهي المنفث المتحكم به الكتروحراريا (TECMN) لغرض الحصول على منفث ذي آداء افضل. مبدأ عمل هذه التقنية هو القيام بتسخين الجدار الجانبي قبل الخانق والتبريد للجدار بعد الخانق لغرض تسخين الغاز ثم تبريده من خلال الجدار حيث يعتقد انه سيحسن من كفاءة واداء المنفث. تسخين و تبريد طرفي الجدار سيكون بواسطة تصنيع الجدار من قطعة الكتروحرارية تعمل حسب مبدأ Peltier. تم حل المعادلة العامة شبهة احادية الاتجاه عدديا في نموذج لمنفث دقيق مع تسخين الغاز الذي يجرى بسرعة تحت السرعة الصوتية وتبريده عندما يكون بسرعة تفوق السرعة الصوتية ووجد تحسن في اداء المنفث. اما الجدار اللالكتروحراري لهذه التقنية فقد تمت دراسته ايضا بصورة مفصلة. فقد تمت كتابة المعادلة التفاضلية لنموذج للجدار ذو شكل غير منتظم المقطع وباعتبار كل الاحمال الحرارية و الكهربائية ومن ضمنها انتقال الحرارة العالي على جانب الجدار. وكذلك تم حل النموذج عدديا وتم حل نموذج منتظم المقطع تحليليا لغرض المقارنة. وتم دراسة النماذج بوجود تغيرات في عوامل رئيسية محسوبة بدون وحدات قياس لغرض معرفة تأثير هذه العوامل على اداء هذه التقنية. لقد تم حل معادلة الجريان الثنائي الابعاد و الخاضعة لقوانين حفظ المادة والطاقة في المنفث الدقيق عدديا و تحت عدة ظروف حدودية على جدار المنفث و هي: جدار الجزء المنفرج ذو دراجة الحرارة الثابتة، و توليد حرارة منتظم داخل جدار المنفث، وتوليد وامتصاص الحرارة بشكل غير منتظم داخل جدار المنفث. وقد اظهرت النتائج عند توليد الحرارة المنتظم تحسنا ملحوظا في قيمة الدفع والاندفاع النوعي و تقليل جريان الغاز وكذلك تحسين كفاءة الاندفاع النوعي للمنفث. عند ظروف توليد وامتصاص الحرارة بشكل غير منتظم في الجدار تم عمل الاختبار ضمن مدى ارقام رينولدز (Re) اقل من 10<sup>3</sup> وكذلك تم حلّ معادلات الغاز احادية البعد للتنبؤ بانتقال الحرارة داخل الجدار ذي المقطع المنتظم. لقد وجد ان التحسن في كفاءة الاندفاع النوعي للمنفث تتزايد بشكل ملحوظ عند ارقام رينولدز تتراوح عند 100 او اقل، و قد وصل التحسن بزيادة قدرها 9.35% عند رقم رينولدز (Re=15) اثناء عملية تسخين و تبريد جدار المنفث. بالاضافة الى انه عملية التبريد و التسخين المزدوج تعطى نتائج افضل من التسخين المنتظم في تقليل والاقتصاد جريان الغاز في المنفث

### **APPROVAL PAGE**

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### DECLARATION

I hereby declare that this thesis is the result of my own investigations, except were otherwise stated. I also declare that it has not been previously and concurrently submitted as a whole for any other degrees at IIUM or other institutions.

Amar Hasan Hameed

Signature.....

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### LIST OF SYMBOLS

- A Cross sectional area  $(m^2)$
- *a* Initial thickness of non-uniform TE (m)
- $A^*$  Throat area (m<sup>2</sup>)
- $A_f$  Area of outlet section (m<sup>2</sup>)
- $A_i$  Area of inlet section (m<sup>2</sup>)
- $C_d$  Discharge coefficient
- $C_p$  Specific heat at constant pressure (kJ/kg.K)
- Cvo Exhaust velocity coefficient
- D Duct diameter (m)
- d Depth (m)
- *f* Friction coefficient
- *fr* Friction coefficient
- $g_o$  Gravitational acceleration (m/s<sup>2</sup>)
- *h* Heat convection coefficient ( $W/m^2$ .K)
- $h_1$  Enthalpy at sections 1 (J)
- *I* Electrical current (Amp)
- $I_{sp}$  Specific impulse (s)

# $I_{sp}^{optim}$

- $I_{sp}^{-}$  Optimum (theoretical) specific impulse (s)
- J Electric current density  $(Amp/m^2)$
- *k* Thermal conductivity (W/m.K)
- $k_A$  Area variation coefficient

Kn	Knudsen number
L	Length (m)
М	Mach number
ṁ	Mass flow rate (Kg/s)
Ν	Number of numerical steps
Р	Perimeter (m)
$P_{input}$	Power input (W)
$p_o$	Stagnation pressure (N/m <sup>2</sup> )
$p_{\infty}$	Ambient pressure (N/m <sup>2</sup> )
<i>p</i> <sub>exit</sub>	Pressure at the exit section $(N/m^2)$
q	Heat flux (W/m <sup>2</sup> )
$Q_{cold}$	Heat absorbed at the cold side (W)
$Q_{hot}$	Heat rejected at the hot side (W)
R	Specific gas constant (J/kg.K)
R <sub>cond</sub>	Thermal conduction resistance (K/W)
R <sub>conv</sub>	Thermal convection resistance (K/W)
Re	Reynolds number
S	Seebeck coefficient (V/K)
Т	Temperature (K)
T <sub>ad</sub>	Adiabatic wall temperature (K)
$T_c$	Cold side temperature (K)
T <sub>gas</sub>	Gas temperature (K)
$T_h$	Hot side temperature (K)
$T_M$	Mean absolute temperature (K)
$T_o$	Gas stagnation temperature (K)

- $T_o^*$  Gas stagnation temperature at throat (K)
- $T_w$  Wall temperature (K)
- *V* Gas velocity (m/s)
- W Wall thickness (m)
- *x* Displacement in x-coordinate (m)
- *y* Displacement in y-coordinate (m)
- Z Figure of merit

### Greek symbols

- $\alpha$  Aspect ratio: length per initial thickness ratio (L/w<sub>o</sub>)
- γ Specific ratio
- $\Delta T$  Temperature difference, T<sub>H</sub>-T<sub>C</sub> (K)
- $\eta_{nozzle}$  Nozzle thermal efficiency
- $\eta_{sp}$  Specific impulse efficiency
- $\lambda$  Thermal conductance (W/K)
- $\mu$  Viscosity (N.s/m<sup>2</sup>)
- $\pi_{ab}$  Peltier coefficient (V)
- $\rho$  Density (kg/m<sup>3</sup>)
- $\rho_{elc}$  Electrical resistivity ( $\Omega$ .m)
- **R** Recovery factor
- $\sigma$  Electrical conductivity (S/m)
- $\tau$  Nozzle thrust (N/m depth)

#### Subscripts

*1* Refers to section one

- 2 Refers to section two
- actu Actual
- ad Adiabatic
- *id* Ideal

### LIST OF ABBREVIATIONS

2D	Two dimensional
3D	Three dimensional
AUSM+	Modified advection upwind splitting method
C.O.P.	Coefficient of performance
DSMC Direct	simulation Monte Carlo
EGR	Energy growing ratio
et al.	(et alia): and others
etc	(et cetera): and so forth
FEM	Finite element Method
F.D.	Fine discrete
FVM, FV	Finite Volume Method
GSFC	NASA/Goddard space flight centre
HRR	Heat resistance ratio
i.e.	that is
MEMSMicro	electro mechanical system
NS	Navier-Stock
R.K.	Runge-Kutta scheme
SPICE	Simulation program with integrated circuit emphasis
TE	Thermoelement
TECMN	Thermoelectrically controlled micronozzle
UDF	User defined function

### **CHAPTER ONE**

### **INTRODUCTION**

#### **1.1 BACKGROUND**

Miniaturization of engineering systems is one of the distinct characteristics of modern industry. With obvious strict limitations on weight and size, space industry is, by no means, an exception. The future of satellite technology advances toward launching increasingly smaller satellites. Small satellites may be classified according to their weight into Micro-satellites (<100 kg), Nano-satellites (<10 kg), and Pico-satellites (< 1 kg). A mission which is typically performed by one big satellite can be done by a group of Nano-satellites with a fraction of the required budget. The number of launched micro and nano-satellites increased during the last two decades, further a significant presence of nano-satellites (< 20 kg) in the past last decade, as the recent statistics given by Cheah and Chin (2011). Those trends in the spacecraft industry are driving the development of low-thrust propulsion systems. These may be needed for fine attitude control or to reduce the mass of the propulsion system through the use of small lightweight and micro scale components. However, MEMS supersonic micronozzle, a key component of micropropulsion systems, has suffered from low efficiency due to viscous effect in micro scale. Micro-scale flow analysis differs from macro-scale one in many aspects. First, the hydrodynamic slip and the thermal temperature jump conditions may arise on the micro-scale level as a consequence of the rarefied gas flow. Secondly, viscous losses are more significant at low Reynolds numbers, and viscous dissipation on a micro-scale level changes the temperature distribution because it works as an energy source, which is induced by the shear stress.

1

This in turn will affect heat transfer rates. Moreover, due to the reduced physical size of microthrusters, surface effects such as friction and heat transfer can dominate the gas flow in such devices, at which may require cooling. In this research, the wall temperature and wall heat fluxes play a significant role in controlling the gaseous flow and thruster performance.

#### **1.2 THERMOELECTRICALLY CONTROLLED MICRONOZZLE**

The effects of area change, friction and heat transfer on compressible flow have been separately considered in the literature. A convergent-divergent nozzle under the effect of heat adding or removing through a thermoelectric wall is configured for better expected performance. Heat exchange with the flow across the nozzle walls is one of the important effects that may have a direct impact on the properties of the flow especially when the surface area-to-volume ratio is high. Thermoelectric effect is proposed to provide heating in the convergent part and cooling in the divergent part of a micronozzle. We call such micronozzle a thermoelectrically controlled micronozzle (TECMN).

Compressible gas flow through a duct, whose cross-sectional area is varying, occurs in many engineering devices, including nozzles. The general effects of area variation on the isentropic flow through a nozzle are derived from the conservation laws, the ideal gas law, and the definition of Mach number. The physical effects of area change on Mach number (M) are summarized as stated by Shapiro (1953);

When M < 1 (subsonic flow), and A increases, M decreases.

When M > 1 (supersonic flow), and A increases, M increases.

When M = 1, dA = 0.

The results above show that if a subsonic flow is to be accelerated to a supersonic velocity it must be passed through a convergent-divergent passage or nozzle. The convergent portion accelerates the flow up to a Mach number of sonic velocity at the throat, and the divergent section then accelerates the flow to supersonic velocity. At the throat, since dA=0, the Mach number is sonic. The duct area at which the critical conditions (sonic velocity) exist is signed as A<sup>\*</sup>, where Mach number M<sup>\*</sup> is equal to (1) at this section.

Heat addition or removal may result, for example, from the heating or cooling of the wall of the duct through which the gas is flowing or from chemical reactions that occur in the flow such as in a combustion chamber or due to evaporation of liquid droplets being carried in the flow. The effect of heating or cooling of the flow appears in changing the stagnation temperature of the flow. The physical changes due to changing stagnation temperature of the flow are shown in the figure below, which is drawn from using the Mach number-stagnation temperature relation explained in Oosthuizen and Carscallen (1997).



Figure 1.1: Variation of stagnation temperature ratio in constant area duct with heat exchange (Rayleigh flow).

It is evident from the Figure 1.1 that, if heat is added to the flow, the Mach number tends towards (1) while if heat is extracted from the flow, the Mach number moves away from (1) in both subsonic and supersonic flow. In other words, heating accelerates the subsonic flow and decelerates the supersonic flow, whereas cooling decelerates the subsonic flow and accelerates the supersonic flow; Figure 1.1.

#### **1.3 THERMOELECTRICITY**

Temperature gradient induces through a thermoelement (TE) supplied to an electrical field at the junctions due to the occurrence of heat pumping from the cold side to the hot side. The lateral surface of the TE is a not isothermal surface due to the temperature gradient within the TE. The temperature at the TE surface drops from hot temperature  $T_H$  to the cold temperature  $T_C$ . Typically, TE is assumed to be insulated on the lateral surfaces. So, heat exchange is normally considered and calculated at the junctions only. The TE planned to be used here is insulated at all lateral surfaces

except the side which is exposed to gas flow. As a result of Peltier effect, the rate of heat pumping at the cold junction ( $T_c$ ) is given by  $\pi_{ab}I$ . Using the Kelvin's relationship ( $S = \pi_{ab} / T_c$ ), we can write;

$$\pi_{ab}I = S \left( T_{M} - \Delta T / 2 \right) I \tag{1.1}$$

Or

$$q = S(T_c) * I \tag{1.2}$$

*S* is the Seebeck effect coefficient ( $S=V/\Delta T$ ) which is measured in V/K or more often in  $\mu v/K$ ,  $T_M$  is the mean absolute temperature ( $T_H+T_C$ )/2 and  $\Delta T$  is the temperature difference  $T_{H}-T_C$  as defined by Rowe (1995).



Figure 1.2: Thermoelectric refrigerator (The Peltier effect), as quoted from Rowe (2006).

The cooling effect at the source junction is opposed by Joule heating in the thermoelement (TE) and by heat conducted from the hot junction to the cold one. Half of the overall Joule heating travels to each of the junctions. Thus, the rate of absorption of heat from the source (at the cold side) is given by;