COPYRIGHT[©] INTERNATIONAL ISLAMIC UNIVERSITY MALAYSIA

SYNTHESIS OF CARBON NANOTUBES ON IMPREGNATED POWDERED ACTIVATED CARBON FOR REMOVAL OF CADMIUM FROM WATER

BY

MOHAMMED A. ABDUL RAHMAN ALSAADI

A thesis submitted in fulfilment of the requirement for the degree of Doctor of Philosophy (Engineering)

> Kulliyyah of Engineering International Islamic University Malaysia

> > **JULY 2011**

ABSTRACT

Water resources are being polluted from various sources. Types of emerging pollutants are also increasing while the traditional pollutants are not solved efficiently yet. Removal of toxic metals is one of the biggest challenges in ensuring safe water for all. Those can be removed by chemical processes, physical processes such as ultra filtration and reverse osmosis, adsorption by polymers and various types of media which exhaust fast and expensive to reactivate. Cadmium (Cd^{2+}) was selected, in the present study, for its potential hazards to living beings at low concentration and difficulties in removing from water. Therefore, due to their high adsorption capacity and high surface area, carbon nanotubes (CNT) were synthesized and used to remove cadmium from water. Fixed catalyst chemical vapor deposition reactor (FCCVD) system was fabricated, upgraded and used to grow carbon nanotubes. Growth parameters (reaction time, reaction temperature, and gas flow rates) for CNT on powdered activated carbon (PAC), as a novel substrate were optimized. The PAC was impregnated with Fe³⁺ catalyst. Design Expert software was used to design the experimental plan and to determine the optimization parameters for the growth of CNT, considering removal (%) of Cd^{2+} as a response. Based on the screening test, four samples were selected for detailed study. Selected CNT-PAC samples were characterized using field emission electron microscope (FESEM) and transmission electron microscope (TEM) to confirm the CNT growth as well as to study the microstructure of the nanoscale product. In addition, the selected CNT-PAC samples were further characterized using Fourier transform spectroscopy (FTIR), thermal gravimetric analysis (TGA) and Brunauer, Emmett and Teller (BET) surface area. The surface properties of CNT-PAC were modified by oxidative functionalization using three different methods: sonication with KMnO₄, refluxing with HNO₃ at 140 °C and in-situ gasification with CO₂ at 750 °C. By comparing the performance, the best modified sample was found to be the one, which was functionalized with KMnO₄. Design Expert software was also used to optimize the removal of cadmium from water with pH, contact time, adsorbent dose and agitation speed as controlling parameters. KMnO₄ treatment of the most promising CNT-PAC sample (B3) enhanced the Cd⁺ removal from 38.87% to 98.35%. Tip growth was observed from TEM. The results showed that BET surface area was 974.9 m²/g, Zeta potential was - 46.1 mV and TGA combustion temperature range was between 371 °C and 560 °C. The selected functionalized sample was used to perform optimization study on removal of Cd²⁺ from water using central composite design (CCD) experimental design. The optimum conditions were pH 4.92, agitation speed 160 rpm, contact time 60 min and adsorbent dose 214 mg/L. Langmuir and Freundlich adsorption isotherms were studied for the novel adsorbent. Langmuir constants were $q_m = 69.759 \text{ mg/g}$, $K_1 = 0.223$ and $R^2 = 0.924$. The system was found more likely to follow Freundlich model with R^2 of 0.961, K_f of 9.215 and n of 3.015. Three kinetic models (pseudo first order, second order and intraparticle adsorption) of adsorption were studied too. The Pseudosecond-order was the best fit with R^2 of 0.996 and model constants were $q_e = 34.29$ (mg/g) and $K_2 = 0.0013$ (g/mg.min). Coefficients for the pseudo first order were q_e = 21.145 (mg/g) and $K_1 = 0.09$ (min⁻¹) with R² of 0.936. The intraparticle kinetic model exhibited R² value of 0.812 with $K_d = 1.295$ (g/mg.min^{0.5}). The CNT-PAC adsorbent after oxidative functionalization with KMnO₄ was proven to be an efficient adsorbent for Cd^{2+} removal from water. Thus this novel nanocomposite material is promising for other adsorption applications for its significant surface properties.

خلاصة البحث

إن موارد المياه تتعرض لمصادر مختلفة من الملوثات. و أنواع الملوثات في زيادة و توسع وليست الطرق الشائعة للتنقية قادرة على ايجاد حلول لهائية لمشاكل التلوث. إن إزالة المعادن السامة من الماء تعد من التحديات الكبرى لتأمين المياه الصحية. عادة ما يتم ذلك باستخدام عمليات كيميائة أو فيزيائية مرتفعة الكلفة مثل الترشيح الفائق الدقة او الضغط الازموزي المنعكس أو البوليمرات بالإضافة إلى استخدام أنواع متعددة من المواد الممتزة و التي تستهلك بسرعة و يصعب أعادة تنشيطها و استخدامها لارتفاع الكلفة. تم اختيار معدن الكادميوم في هذة الدراسة لشدة خطورته على البشر و البيئة. ولذلك تم تحضير و تطوير مادةالانابيب النانو كاربونية لارتفاع قيمة مساحتها السطحية و سعتها الامتصاصية كي تستخدم لإزالة معدن الكادميوم من الماء. و لأجل ذلك تم تصنيع و تطوير منظومة مفاعل كيميائي تحليلي تبخيري ذو عامل مساعد ثابت كي تنمو فيه أنابيب الكربون النانوية (PAC-CNT). تمت دراسة (زمن التفاعل،و درجة حرارة التفاعل و نسبة خلط الغازات المستعملة الاسيتيلين إلى الهيدروجين) و هي ظروف و عوامل لنمو الانابيب النانوية الكربونية فوق سطح الفحم المنشط المسحوق كمادة جديدة. وهذا الكربون ا و الفحم المنشط قد حمل بأيونات الحديدالثلاثي التكافؤ Fe³⁺ ليتخذ عاملا مساعدا على التفاعل. وقد استخدم البرنامج الحاسوبي Design Expert لتصميم مخطط التجارب المختبرية للحصول على أفضل قيمة لكل واحدة من عوامل التفاعل على أن تتحقق في المنتوج أفضل كمية نمو مع أفضل قدرة على إزالة معدن الكادميوم. ومن خلال نتائج المسح الأولية تم اختار أربعة نماذج كي تدرس بالتفصيل. لقد فحصت خواص المادة الناتجة باستخدام FESEM و TEM لتأكيد نمو الأنابيب النانوية و دراسة التركيب السطحي الدقيق لها. اجريت فحوصات الأشعة تحت الحمراء ب FTIR و السلوك الحراري باستخدام TGA بالاضافة الى فحص المساحة السطحية بواسطة (BET). تم تحسين خواص سطح المتج (CNT- PAC) بتفعيله بالأكسدة لتثبيت محموعات كيميائية فعالة بثلاث طرق: المزج بالموجات فوق الصوتية مع ال KMnO₄ و التقليب في حامض النيتريك و الأكسدة بغاز ثاني اوكسيد الكربون بدرجة حرارة 750 مئوية. قورنت النماذج فكان أحسنها أداءا تلك التي عوملت بالKMnO₄. درست خواص المنتج النهائي فظهر أن النمو كان نموا طرفيا بالنسبة لأنابيب النانو من خلال الTEM. بينت النتائج الاخرى أن المساحة السطحية (BET) بلغت 974.9 m²/g و أن الجهد زيتا (Zeta potential) بلغ1.64 − WV و مدى الاحتراق كان (°C (371 °C) إلى (560 °C). النموذج المختار و المفعل السطح استعمل في إزالة ال Cd^{2+} من الماء وقد كان التطور في القدرة على الازالة واضحا اذا ما قورنت النماذج المفعلة السطح بتلك التي لم يفعل سطحها قافزا من 38% إلى 98.35% أجريت عملية المفاضلة لاختيار أفضل الظروف لتفاعل الامتصاص وقد درست العوامل الآنية: pH و زمن التفاعل و حرعة المادة الممتزة و سرعة المزج فوجد أن أفضل القيم pH 4.92 والزمن 60 دقيقة و السرعة 160 دورة بالدقيقة و الجرعة 214 ملغرام باللتر. ولقد درست الأيزوثرم حسب (Langmuir) و R²=0.961, K_f=) فكانت ثوابتها (R² 0.924. q_m 69.759 mg/g, K₁ 0.223) للأول و (Freundlich) Pseudo) للثاني فكان هوخير ما يمثل النظام. ثم درست حركية التفاعل الامترازي حسب ال(9.215 and n =3.015 q_e و ال (first order) و ال (Pseudo-second-order) و كانت الثواب $R^2 = 0.996$ و first order) و ال تساوي 34.29 (mg/g) و $K_2 = 0.0013$ (g/mg.min) و $K_2 = 0.0013$ (g/mg.min) و ذلك للنمط الثاني الذي مثل النظام خيرا من النمطين الاخرين. الذان كانت ثوابتهما كما يأتي: للنمط الأول (R²=0.936) و (K₁= 0.09 (min⁻¹) و R (mg/g) =21.145 (g/mg.min^{0.5}) و ثوابت التداخل الجزيئي كانت R²= 0.812 و (g/mg.min^{0.5}). ان المتتج (PAC-CNT) قد أبدى أداءًا متميزًا في الامتزاز مما جعل منه مادة واعدة في حال استخدامها لأغراض الامتزاز المتنوعة.

APPROVAL PAGE

The Thesis of Mohammed A. Abdul Rahman has been approved by the following:

Abdullah Al Mamun Supervisor

Suleyman Aremu Muyibi Co-Supervisor

Ahmad Tariq Jameel Internal Examiner

Nassereldeen Ahmed Kabashi Internal Examiner

> Mohd Omar Ab. Kadir External Examiner

Momoh Jimoh Eyiomika Salami Chairman

DECLARATION

I hereby declare that this dissertation is the result of my own investigations, except where otherwise stated. I also declare that it has not been previously or concurrently submitted as a whole for any other degrees at IIUM or other institutions.

Mohammed A. Abdul Rahman

Signature _____

Date _____

INTERNATIONAL ISLAMIC UNIVERSITY MALAYSIA

DECLARATION OF COPYRIGHT AND AFFIRMATION OF FAIR USE OF UNPUBLISHED RESEARCH

Copyright © 2011 Mohammed A. Abdul Rahman. All rights reserved.

SYNTHESIS OF CARBON NANOTUBES IMPREGNATED ON PODERED ACTIVATED CARBON FOR REMOVAL OF CADMIUM FROM WATER

No part of this unpublished research may be reproduced, stored in a retrieval system, or transmitted, in any form or by any means, electronic, mechanical, photocopying, recording or otherwise without prior written permission of the copyright holder except as provided below.

- 1. Any material contained in or derived from this unpublished research may only be used by others in their writing with due acknowledgement.
- 2. IIUM or its library will have the right to make and transmit copies (print or electronic) for institutional and academic purposes.
- 3. The IIUM library will have the right to make, store in a retrieval system and supply copies of this unpublished research if requested by other universities and research libraries.

Affirmed by Mohammed A. Abdul Rahman.

Signature

Date

ACKNOWLEDGEMENTS

In the name of Allah, the Most Gracious and the Most Merciful.

In the first place, all the praises and thanks are to Allah Almighty for granting us success in this work. Praise to Allah Almighty for giving us patience and strength to complete this study as a fulfillment of the requirement of Doctorate of philosophy in Biotechnology Engineering successfully.

The author would like to extend his sincere thanks and gratitude to the chairman of the supervisory committee, Associate Professor Dr. Abdullah Al-Mamun for his continued support, supervision, encouragement and valuable guidance throughout the duration of this research study. The author wishes to express his profound appreciation and gratitude Prof. Dr. Suleyman Aremu Muyibi for his support, excellent guidance and valuable suggestions. Many thanks also extended to the other members of the supervisory committee, Prof. Md. Zahangir Alam and Associate Prof. Dr Iis Sopyan for their constructive suggestions and valuable comments and extended thanks to the staff of analytical and bioinstrumentation lab., Assoc. Prof. Dr. Mohammed El-Wathig for his useful advices and Senior Lab Assistant Br. Hj Sukiman for his efforts and experience in analytical work and in the success of this research. Appreciation and thanks to the staff of Biotechnology Engineering Department for their continuous support. and appreciations also to Material and Manufacturing Engineering Department for the support and cooperation in their analytical and characterization labs.

Deep appreciation is also given to Prof. Dr Momoh Jimoh Eyiomika Salami, Deputy Dean of Postgraduate & Research and his staff for their kind cooperation. High appreciation goes to the personnel in the Center of Post-graduate Studies, IIUM.

The author presents thankfulness and gratitude to Prof. Ir. Dr. Mohd Omar Ab. Kadir, Assoc. Prof. Dr. Ahmad Tariq Jameel and Assoc. Prof. Dr. Nassereldeen Ahmed Kabashi for their valuable guidance and important observations.

Finally the author presents his most sincere thanks and warmest gratitude to his father Prof. Sh. Dr. Abdul Hakeem Al Saadi and his mother as well (may Allah SWT bless and reward them). The warm gratitude and thanks are extended to Prof. Sh. Dr. Abdul Razzaq Al Saadi and all other family members, especially author's wife and children for their support during study period.

TABLE OF CONTENTS

Abstract	ii
Abstract in Arabic	iii
Approval Page	iv
Declaration Page	v
Copyright Page	vi
Acknowledgements	vii
List of Tables	xii
List of Figures	XV
List of Abbreviations	xxi

CHAPT	ER ONE INTRODUCTION	1
1.1 C	OVERVIEW	1
1.2 P	PROBLEM STATEMENT AND SIGNIFICANCE OF STUDY	2
1.3 R	RESEARCH PHILOSOPHY	3
1.4 R	RESEARCH OBJECTIVES	4
1.5 R	RESAERCH METHODOLOGY	5
1.6 C	DRGANIZATION OF THE THESIS	6

CHAP	TER TWO LITERATURE REVIEW	8
2.1	INTRODUCTION	8
2.2	CARBON NANOTUBES	8
	2.2.1 Structure of Carbon Nanotubes	9
	2.2.2 Growth of CNT	16
	2.2.3 Chemical Properties of CNT	20
	2.2.4 Production Methods of Carbon Nanotubes	24
	2.2.4.1 Arc Discharge	25
	2.2.4.2 Laser Ablation	27
	2.2.4.3 Chemical Vapor Deposition (CVD)	29
	2.2.4.3.1 Advantages of CVD	31
	2.2.4.3.2 Vapor Phase Growth	32
	2.2.4.3.3 CVD Substrate Catalyst Method	37
	2.2.4.3.4 Influence of Metal Catalyst In CVD Method	41
	2.2.4.3.5 Influence of Particle Size In CVD Method	43
	2.2.4.3.6 Fluidized-Bed Cvd Method	45
	2.2.4.4 Plasma Enhanced Chemical Vapor Deposition	48
	2.2.5 Functionalization of CNT	52
2.3	HEAVY METALS IN WATER	58
	2.3.1 Cadmium	59
	2.3.1 Adsorption of Heavy Metals	62
	2.3.1.1 Zeta Potential of The Adsorbents	62
	2.3.1.2 Adsorbent Surface Area	63

		2.3.1.3	Adsorption Isotherm	. 65
		2.3.1.3	3.1 Freundlich Isotherm	. 66
		2.3.1.3	3.2 Langmuir Isotherm	. 67
		2.3.1.4	Adsorption Kinetics	. 70
		2.3.1.4	4.1 Pseudo-First-Order Adsorption Kinetics	. 70
		2.3.1.4	4.2 Pseudo-Second-Order Adsorption Kinetics	. 72
		2.3.1.4	4.3 Intraparticle Diffusion Kinetics	. 73
2	2.4	SUMMARY	OF LITERATURE REVIEW	. 74
CH	[AP	TER THREE	E MATRIAL AND METHODOS	. 75
3	5.1	INTRODUCTIO	N	. 75
3	5.2	MATERIALS		. 76
		3.2.1 Chemi	icals	. 76
		3.2.2 Gases		. 77
3	5.3	EQUIPMEN	Γ	. 77
		3.3.1 Equip	ments Used for Synthesis of CNT-PAC	. 77
		3.3.1.1	CVD Reactor	. 77
		3.3.1.2	Tubular furnace	. 77
		3.3.1.3	Trinder	. 78
		3.3.1.4	Drier Oven	78
		3315	Reflux System	78
		3316	Ultrasonication	78
		3317	Vacuum Filtration	78
		332 Equir	ments Used for Characterization and Testing	79
		3321 I	nH meter	79
		3322	Atomic Absorption Spectrometer (AAS)	79
		3323	Surface Area and Pore Size Measurement (BET Isotherm)	79
		3324	FESEM	. 70
		3.3.2.4		. /9 00
		3.3.2.3	Τ ΕΙΝΙ Τ Ο Δ	. 00
		3.3.2.0		. 80
2		3.3.2.7	F11K	. 80
3	.4	METHODS		. 80
		3.4.1 Gener	ral Research Plan Flow Chart	. 80
		3.4.2 CVD	Reactor Modification and Fabrication	. 81
		3.4.3 Catal	yst Preparation and Selection	. 86
		3.4.3.1	Preparation of Powdered Activated Carbon (PAC)	. 87
		3.4.3.2	Impregnation of Iron (iii) on PAC	. 87
		3.4.3.3	Selection of Catalyst Composition	. 88
		3.4.4 Produ	ction of Carbon Nanotubes on Powdered Activated Carbon	. 88
		3.4.4.1	Design of Experiment (DOE) For CNT Synthesis on PAC	. 90
		3.4.4.2	Response of CCD for CNT Synthesis Optimization	. 92
		3.4.5 Chara	cterization of the Product	. 92
		3.4.6 Modif	ication of CNT-PAC	. 94
		3.4.6.1	Insitu-oxidization of CNT-PAC Using CO ₂	. 94
		3.4.6.2	Oxidation with Nitric Acid HNO ₃	. 94
		3.4.6.3	Oxidation with Potassium Permanganate KMNO ₄	. 95
		3.4.6.4	Comparison with PAC and Commercial MWCNT	. 95
		3.4.7 Optim	ization of Removal of Cadmium	. 95
		1		

	3.4.8 Adsorption Isotherm Study	. 97
	3.4.8.1 Freundlich Isotherm.	. 99
	3.4.8.2 Langmuir Isotherm	. 99
	3.4.9 Adsorption Kinetics	. 100
	3.4.9.1 Pseudo-First-Order	. 100
	3.4.9.2 Pseudo-Second-Order	. 101
	3.4.9.3 Intraparticle Diffusion Model	. 101
3.5	SUMMARY OF METHODOLOGY	. 101
		
CHAP	TER FOUR RESULTS AND DISCUSSIONS	. 103
4.1		. 103
4.2	IMPROVEMENT OF THE CVD REACTOR	. 103
	4.2.1 Gas Leak Control and Assembly Time	. 103
	4.2.2 Cooling of Furnace after Reaction	. 106
1.0	4.2.3 Summary of First Objective	. 107
4.3	SELECTION OF CATALYST AMOUNT	. 107
4.4	SCREENING OF CNTS SYNTHESIS CONDITIONS	. 113
	4.4.1 Design of Experiment (DOE) for Production of CNT-PAC	
	Samples	. 113
	4.4.2 Production of CNT-PAC Samples	. 116
	4.4.3 Adsorption of Cd ² for Screening	. 116
	4.4.4 Statistical Analysis for the Screening of Adsorbent	. 117
	4.4.4.1 Analysis of Variance (ANOVA) for Set A	. 117
	4.4.4.2 Analysis of Variance (ANOVA) for Set B	. 120
	4.4.5 Summary of optimization the conditions of CNT-PAC synthesis	. 130
4.5	OXIDATIVE FUNCTIONALIZATION OF CNT- PAC OPTIMUM	
	SAMPLES	. 131
	4.5.1 Comparative Study of CNT-PAC Functionalization	. 131
	4.5.2 Summary of Functionalization Findings	. 139
4.6	CHARACTERIZATION OF THE CNT- PAC SAMPLES	. 140
	4.6.1 FESEM Images	. 140
	4.6.2 TEM Images	. 147
	4.6.3 Surface Area and Pore Size Analysis for CNT-PAC	. 151
	4.6.4 Zeta Potential of the Adsorbents	. 154
	4.6.5 Thermo Gravimetric Analyses (TGA)	. 155
	4.6.6 Surface Chemistry of the Adsorbents	. 158
	4.6.7 Summary of Characterization	. 161
4.7	OPTIMUM CODITIONS FOR CADMIUM ADSORPTION	. 162
	4.7.1 Design of Experiment (DOE) for Optimization of Cd^{2+} Removal	. 162
	4.7.1.1 Statistical Analysis for Cd^{2+} Removal from Water by Modif	ied
	CNT-PAC	. 164
	4.7.1.1.1 Analysis of Variance (ANOVA)	. 164
	4.7.1.2 Effect of Optimization Variables on Adsorption of Cd^{2+}	. 170
4.8	ADSORPTION ISOTHERM AND KINATIC STUDIES	. 175
	4.8.1 Adsorption Isotherms	. 175
	4.8.2 Adsorption Kinetics	. 179
4.9	SUMMARY	. 185

CHAI	PTER FIVE CONCLUSIONS AND RECOMMENDATIONS	188
5.1	CONCLUSIONS	188
5.2	RECOMMENDATIONS	190

BIBLIOGRAPHY 1	19)2	2
----------------	----	----	---

APPENDIX A	14
APPENDIX B	18
APPENDIX C	23
APPENDIX D	41
APPENDIX E	4 9

LIST OF TABLES

<u>No</u> 2.1	Summary of Synthesis of CNT Using CVD Techniques	<u>Page</u> 47
2.2	Cd ²⁺ Adsorption Capacities of Various Adsorbents	61
3.1	Weights of Iron Nitrate and Activated Carbon Used in Preparing Catalyst Samples	86
3.2	Set A Lower and Upper Limits for CCD Experiments Design to Synthesize CNT on PAC with CVD	90
3.3	Set B Lower and Upper Limits for CCD Experiments Design to Synthesize CNT on PAC with CVD	90
3.4	CCD Runs Layout Stating Values of Different Operating Parameters for CNT Production on PAC by CVD (Set A)	91
3.5	CCD Runs Layout Stating Values of Different Operating Parameters for CNT Production on PAC by CVD (Set B)	91
3.6	Optimization Parameters of Water Treatment Application	96
3.7	Parameters of Experimental CCD for Optimization of Cd ²⁺ Removal by CNT-PAC Using Design Expert 6.0 Software	97
3.8	Kinetics Models Forms and Parameters	101
4.1	Results of the Catalyst Amount Selection Process	108
4.2	CCD of Experiment for Production Parameters of CNT-PAC Set A	114
4.3	CCD Of Experiment for Production Parameters of CNT-PAC Set B	115
4.4	Production Conditions of Selected CNT-PAC Samples Those Subjected to Surface Modification	120
4.5	Response Surface Reduced Quadratic Model Analysis of Variance (ANOVA) for the Yield of CNT Growth (Set B Data)	121
4.6	Constants of Regression Equation for Yield (Set B)	122
4.7	Response Surface Reduced Quadratic Model Analysis of Variance (ANOVA) for %Removal of Cd ²⁺ (Set B Data).	126

4.8	Constants of Regression Equation for Cd ²⁺ removal (Set B)	126
4.9	Constrains for Optimization of Production Conditions for CNT-PAC for Removal of Cd^{2+} (Set B)	127
4.10	Solutions of Set B for The Optimum Conditions of CNT Growth	127
4.11	Adsorption Capacities and Removal of Different Surface Modified Adsorbents	134
4.12	Comparative BET Results Summery for CNT-PAC, Commercial CNT PAC And Calcinated Fe /PAC	152
4.13	Zeta Potential of Different Carbon Material Samples in Deionized Water	155
4.14	TGA Data Obtained from Thermo Gravimetric Analyses of (A) CNT-PAC, (B)PAC, (C) Commercial Mwcnts	157
4.15	Peaks and Functional Groups Detected by FTIR on CNT-PAC	160
4.16	Summary of Central Composite Design of Experiment or Parameters of Removal of Cd^{2+} by Modified CNT-PAC	of 163
4.17	CCD of Experimental Parameters of Removal for the Cd ²⁺ by CNT-PAC	Modified 164
4.18	Responses CCD Experiment for Removal of Cd ²⁺ by Modified CNT-PAC	164
4.19	Reduced Quadratic Model Analysis of Variance (ANOVA) for Cd ²⁺ Uptake Capacity on CNT-PAC	166
4.20	Reduced Quadratic Model Analysis of Variance (ANOVA) for $Cd^{2+} Rd^{2+}$ by CNT-PAC	emoval 167
4.21	Constants of Regression Equation of CCD for Cd^{2+} Adsorption by CNT-PAC Equations 4.10 and 4.11	168
		100
4.22	Constraints for Optimization Process Based on CCD for Cd ²⁺ Removal	168
4.224.23	Constraints for Optimization Process Based on CCD for Cd ²⁺ Removal Potential Optimization Conditions Based on CCD for Cd ²⁺ Removal	168 168
4.224.234.24	Constraints for Optimization Process Based on CCD for Cd ²⁺ Removal Potential Optimization Conditions Based on CCD for Cd ²⁺ Removal Adsorption Isotherm Models for CNT-PAC Comparing with Different Adsorbents	168 168 179

LIST OF FIGURES

<u>No.</u> 1.1	Flow Chart of Research Methodology	Page 6
2.1	Image of MWCNT (Gogotsi, 2006)	10
2.2	Construction of CNT	11
2.3	Patterns of CNT twist. (a) Zigzag Single-Walled Nanotube. Note the zigzag pattern around circumference and $m = 0$. (b) Armchair Single-Walled anotube. Note the chair-like pattern around circumference and $n = m$ (c) Chiral Single-Walled Nanotube. Note twisting of hexagons around tubulebody. (Gogotsi & Corporation, 2006; Harris, 2001)	13
2.4	Schematic illustrations of the chiral structures of CNT, (A) armchair, (B) zigzag, and(C) chiral SWNTs. Projections normal to the tube axis and perspective views along the tube axis are on the top and bottom, respectively. (D) Tunneling electron microscope image showing the helical structure of a 1.3-nm-diameter chiral SWNT. (E) Transmission electron microscope (TEM) image of a MWNT containing a concentrically nested array of nine SWNTs. (F) TEM micrograph showing the lateral packing of 1.4-nm-diameter SWNTs in a bundle. (G) Scanning ectron microscope (SEM) image of an array of MWNTsgrown as a nanotubeforest (Ray et al., 2002).	13
2.5	Diagram showing rolling direction of nanotube (Dresselhaus et al., 1998).	14
2.6	Structures of carbon nanotubes (www.iljinnanotech.co.kr,2002).	15
2.7	TEM images for different structures of MWCNT.	16
2.8	Growth of carbon fibers and tubes	18
2.9	Reversible gasification/growth of carbon filaments from nickel particles. (Figuelredo et al, 1990)	19
2.10	The three possible adsorption sites on a bundle of SWNTs with closed ends. (Babaa et al., 2004, and Rakov, 2006.)	l 22
2.11	Schematic diagram of arc-discharge apparatus (www.iljinnanotech.co.kr, 2002).	27
2.12	Schematic drawings of a laser ablation apparatus (www.iljinnanotech.co.kr, 2002).	28

2.13	TEM images of a bundle of SWCNT produced with ablation of laser	29
2.14	Schematics drawings of a CVD deposition oven (www.isr.umd.edu, 2003).	31
2.15	Schematic diagram of a vapor phase growth apparatus (www.iljinnanotech.co.kr, 2002).	33
2.16	Schematic diagram of thermal CVD apparatus (www.iljinnanotech.co.kr, 2002)	38
2.17	Schematic diagram of spurting machine (www.angstromsciences.com, 2002).	39
2.18	Schematic diagram of the fluidized-bed reactor (Mauron et al., 2003).	45
2.19	Schematic diagram of Plasma Enhanced CVD apparatus (www.iljinnanotech.co.kr, 2002).	50
2.20	Schematic of a PECVD set-(Yu & Meyyapan, 2006)	51
2.21	Stone–Wales (or 7-5-5-7) defect on the sidewall of a nanotube	54
2.22	Atomic structure and electron density of functional group on CNT (left) of COOH-attached (6,6) SWNT and contour plot of electron density (right) on the slice passing through the COOH group. Red, yellow, green, and blue colors on the contour plot indicate electron density from higher density to lower density. The structural distortion on the nanotubes is found to confine to the nearest neighbors of the bonding site.	56
2.23	Types of isotherms proposed by BET	64
2.24	Freundlich adsorption isotherm linear representation.	67
2.25	Langmuir adsorption isotherm	68
2.26	Pseudo-First-Order Adsorption Kinetics	71
2.27	Pseudo-Second-Order Adsorption Kinetics	72
2.28	Intraparticle diffusion adsorption kinetics	73
3.1	Flow chart of research methodology	81
3.2	The Modified Multi Stage System	82
3.3	Schematic diagram of CNT Multipurpose Triple Stage CVD System.	83
3.4	Control panel for the CVD modified reactor	84

3.5	The bubbling arrangement and the flask of Benzene	86
3.6	Freundlich adsorption isotherm linear representation.	99
3.7	Langmuir adsorption isotherm	100
4.1	CVD-Reactor with two stages and fixed catalyst in the heating zones	104
4.2	Closing cap at with fixing assembly of system	106
4.3	Cooling system	107
4.4	Diameter (nm) distributions of CNT on PAC at different percentage of Fe^{3+} impregnation	109
4.5	Yield of carbon deposited in terms of increase of sample weight versus the percentage of Fe^{3+} impregnation	110
4.6	Coverage percentages of CNT on PAC at different percentage of Fe^{3+} impregnation	111
4.7	PAC impregnated with Fe ³⁺ after calcination and before CNT growth.	112
4.8	Different magnification FSEM Image for CNT-PAC using Benzene as a source of carbon with 1% Fe ³⁺ catalyst impregnation ratio	112
4.9	Different magnification levels of FSEM Image for CNT-PAC using Benzene as a source of carbon with 3% Fe ³⁺ catalyst impregnation	112
4.10:	Different magnification levels of FSEM Image for CNT-PAC using Benzene as a source of carbon with 5% Fe ³⁺ catalyst impregnation	113
4.11	Different magnification levels FSEM Image for CNT-PAC using Benzene as a source of carbon with 7% Fe ³⁺ catalyst impregnation ratio.	113
4.12	Removal of Cd ²⁺ from water by samples of CNT-PAC set A	118
4.13	Removal of Cd ²⁺ from water by samples of CNT-PAC set B	119
4.14	3-D surface response representation of yield of CNT growth versus time(min) and temperature (°C) for set B data	123
4.15	3-D surface response representation of yield of CNT growth versus gas ratio C_2H_2/H_2 and temperature (°C) for set B data.	123
4.16	Validation of yield Equation for set B	124

4.17	3-D surface response representation of Removal of Cd ²⁺ versus time (min) and temperature (°C) at gas ratio 0.1 for set B data.	128
4.18	3-D surface response representation of Removal of Cd^{2+} versus gas ratio C_2H_2/H_2 and temperature (°C) at time 60 minfor set B data	129
4.19	3-D surface response representation of Removal of Cd^{2+} versus time (min) and gas ratio C_2H_2/H_2 at temperature 650 °C for set B data	129
4.20	validation of Removal of Cd^{2+} Equation for set B optimization of production	130
4.21	Removal of Cd ²⁺ from water using four different samples of as grown CNT-PAC	132
4.22	Removal of Cd^{2+} from water using Modified CNT-PAC with HNO ₃	133
4.23	Removal of Cd^{2+} from water using modified CNT-PAC with KMnO ₄	1355
4.24	Removal of Cd^{2+} from water using commercial CNT as grown, oxidized with HNO ₃ and KMnO ₄ .	1366
4.25	Removal of Cd^{2+} from water using Palm Kernel PAC as row, oxidized with HNO ₃ and KMnO ₄	1376
4.26	Removal of Cd ²⁺ by treated and raw adsorbents	138
4.27	FESEM high magnification images for samples (a) A1, (b) A2, (c) A3, (d) A4	141
4.28	FESEM high magnification images for samples (e) A5, (f) A6, (g) A7, (h) A8	142
4.29	FESEM high magnification images for samples (i) A9, (j) A10, (k) A11& (l) A12	143
4.30	FESEM high magnification images for samples (a) B1, (b) B2, (c) B3 & (d) B4	144
4.31	FESEM high magnification images for samples (e) B5, (f) B6, (g) B7, (h) B8	145
4.32	FESEM high magnification images for samples (i) B9, (j) B10, (k) B11, (l) B12	146
4.33	TEM high magnification images for samples B1.	148
4.34	TEM high magnification images for samples B2	149

4.35	TEM high magnification images for samples B4	150
4.36	BET isotherm plot volume of adsorbed N ₂ on surfaces of CNT- PAC, commercial MWCNT, PAC and calcinated Fe-PAC. Versus relative pressure P/Po (adsorption pressure/saturated vapor pressure)	153
4.37	Plot of liner form of BET Equation for CNT-PAC, commercial MWCNT, PAC and calcinated Fe-PAC	154
4.38	TGA Thermo gravimetric analyses under air flow for (a) CNT- PAC, (b) PAC, (c) Commercial MWCNT	157
4.39	FTIR spectra for CNT-PAC before surface oxidation	161
4.40	FTIR spectra for CNT-PAC after surface oxidation with KMnO ₄	161
4.41	Theoretical Vs Experimental Cd^{2+} uptake (Optimization process conditions for Cd^{2+} on CNT-PAC)	169
4.42	3-D surface response representation of Cd^{2+} uptake q (mg/g) and %removal versus pH-time interaction	171
4.43	3-D surface response representation of Cd^{2+} uptake q (mg/g) and %removal versus pH-Dose interaction	172
4.44	One factor plot for response representation of Cd2+ removal (%) by CNT-PAC versus Agitation Speed -Dose interaction	173
4.45	Adsorption uptake of Cd2+ Capacity (qt) on modified CNT-PAC versus Contact Time (t) with various Cd^{2+} Solution initial concentrations	s 176
4.46	Freundlich linear form for Cd ²⁺ adsorption on CNT-PAC in water	177
4.47	Langmuir isotherm linear form for Cd^{2+} adsorption on CNT-PAC in water.	178
4.48	Pseudo first order adsorption kinetics at different initial concentrations, the initial concentration in (mg/L)	181
4.49	Pseudo second order adsorption kinetics at different initial concentrations, the initial concentration in (mg/L)	182
4.50	Intraparticle adsorption kinetics at different initial concentrations, the initial concentration in (mg/L)	183

LIST OF ABBREVATIONS AND SYMBOLS

AC	Activated Carbon
ANOVA	Analysis of Variance
BET	Brunauer–Emmet–Teller
CCD	Central Composite Design
CVD	Chemical Vapor Deposition
DE	Design Expert
DOE	Design of Expert
CNT	Carbon Nanotube
CNT-PAC	Carbon Nanotube Grown on Powdered Activated Carbon
FCCVD	Fixed Catalyst Chemical Vapor Deposition
FESEM	Field Emission Scanning Electron Microscope
FTIR	Fourier Transforms Infrared
MWCNT	Multi Wall Carbon Nanotube
SWCNT	Single Wall Carbon Nanotube
PAC	Powdered Activated Carbon
SEM	Scanning Electron Microscope
TEM	Transmission Electron Microscope
TGA	Thermo gravimetric analysis
C_0	Initial Concentration
Ct	Concentration at Time t
K _L	Langmuir Adsorption Constant
K_F	Freundlich Isotherm Constant
1/n	The Intensity Parameter in Freundlich Isotherm
K ₁	Rate Constant of Pseudo-First-Order
K ₂	Rate Constant of Pseudo-Second-Order Adsorption Kinetics
K _d	Rate Constant of Intraparticle Diffusion
m	Weight of Adsorbent
q _e	Equilibrium Adsorption Capacity
q _t	Adsorption Capacity at time t

- q_m Maximum Adsorption Capacity
- R² Correlation Coefficient
- V Volume of Solution
 - Yield

Y

CHAPTER ONE

INTRODUCTION

1.1 OVERVIEW

Carbon nano materials (CNM) are being globally in the limelight as a new material in the 21st century and broadening their applications have been broadened in many areas, such as biotechnology, environmental energy, aerospace science, materials industry, medicine science, electronic computer, security and safety. CNM are known to be superior to many other existing materials in terms of strength, electrical properties, weight, size, etc. Carbon nanotubes (CNT) can be described as a rolled up one graphene sheet that is closed at each end with half of a fullerene denoted as single walled carbon nanotube, or more than one graphene cylinder nested one into another in case of multi walled carbon nanotubes - MWCNT (Delzeit et al., 2002; Dresselhaus et al., 2001; Stampfer et al., 2006). Among various types of CNM, carbon nanotubes (CNT) are in high demand especially in the following applications (Andrews et al., 2002; Popov, 2004; Tanaka et al., 1999).

- a. Elevation of the existing electron emission current from 10 to 100 times level, using a low voltage;
- b. High functional composites which can drastically enhance the strength of structures;
- c. Various nanotechnologies; and
- d. Bioenvironmental applications, such as pollutant removal, drug delivery, biosensors.

The potential benefits of the synthesis of nano-sized particles for remediation

systems are the technology is portable, the nanoparticles are highly reactive and it can be scaled to contribute in resolving the pollution problems. Furthermore, it also has been found that carbon nanotubes can be used as an adsorbent for trapping volatile organic compounds (VOCs) and heavy metals from environmental samples (Feng et al., 2005). Many researchers as well as academic institutes dedicated great effort to it. CNT is a promising material especially in the field of remediation of toxic heavy metals contaminated industrial waste waters (Li et al., 2003; Liu et al., 2005; Lu & Chiu, 2006; Yantasee et al., 2007).

1.2 PROBLEM STATEMENT AND SIGNIFICANCE OF STUDY

Water resources are being polluted from various sources. Different types of emerging pollutants have been increasing while the removal of traditional pollutants is not solved efficiently yet. Cadmium is one of the most toxic metals, it is ranked the 6th of ten most toxic metals for its dangerous impacts on human health . Toxic metals (such as cadmium, lead, mercury, etc.) are becoming common in water. They are being removed by chemical processes or costly physical processes such as ultra filtration, reverse osmosis, polymers and various types of adsorbing media which exhaust very fast and costly to reactivate. Removal of toxic metals by adsorption is known technique. Adsorption is also related to the accessible surface area of the media. Therefore the CNT with high surface area could be potential to remove toxic metals for the production of high purity water.

Heavy metals are hazardous for the environment and human health as well. Due to high adsorption capacity, CNT are promising material to be applied in the environmental remediation to obtain water free from toxic metals (Atieh et al., 2005; Chen & Wang, 2006; Muataz et al., 2010). Many industrial and medical applications need ultra pure water for their products. Therefore, it is timely to conduct study on development of new materials to produce pure water for human consumption (Colt, 2006; Gil et al., 2006; Gomez et al., 2007; Koster et al., 2002).

In recent years, work has focused on developing Chemical Vapor Deposition (CVD) techniques using catalyst particles and hydrocarbon precursors to grow nanotubes; such techniques have been used earlier to produce hollow nanofibers of carbon in large quantities. CVD seems to be the most promising method for possible industrial scale-up due to the relatively low growth temperature, high yields and high purities that can be achieved (Cheol et al., 2002; Danafar et al., 2009; Dresselhaus et al., 2001; Kukovecz et al., 2005).

The catalyst substrate and floating catalytic chemical vapor deposition (FC-CVD) are very promising processes with respect to large-scale production of different kinds of carbon nanostructures materials as for example vapor growth carbon fibers, carbon nanofibers, multi, and single-walled carbon nanotubes. However, research is necessary to produce quantity of CNT at lower cost. There is also need to study the synthesis of CNT on low cost substrate for the immobilization process. Due to their attractive mechanical, thermal and electronic properties, researchers were more focusing on applications of CNT in other than water treatment fields where the cost plays major role (Zhong et al., 2007).

1.3 RESEARCH PHILOSOPHY

This research is an attempt to benefit from the CNT's physical and chemical properties in the field of environment (specifically water treatment), as one of the greatest challenges that facing the humanity in this century is the conservation of the water resources.

High surface area and presence of functional groups affect the adsorption properties of any adsorbent. Activated carbon (AC) is a well-known adsorbent for the removal of heavy metals despite its limited utility after the adsorption process. The synthesis of nanomaterial on PAC will therefore increase its surface functional groups and give longer span to its activity for the removal of heavy metals. The growth of carbon nanotubes (CNT) on the surface of powdered activated carbon (PAC) is thought to increase the adsorption capacity of the PAC and then the removal of cadmium from aqueous solutions.

1.4 RESEARCH OBJECTIVES

The objectives of this research are:

- To design and fabricate a fixed catalyst chemical vapor deposition reactor (FCCVD) system for the production of CNT.
- To optimize the growth of CNT on powdered activated carbon (PAC) by varying process parameters such as reaction time, reaction temperature, carrier gas flow rate and carbon source gas flow rate.
- To optimize the removal of Cd²⁺ from water, with CNT on PAC dose, contact time, pH and initial concentration of pollutant as controlling parameters.
- 4. To investigate the isothermal adsorption behavior as well as the adsorption kinetics for the process of Cd²⁺ adsorptions in aqueous solution by impregnated CNT grown on PAC and determine the matching isotherm and kinetic models.